

PRESSURE OPERATED PUMP POP

(1" x 1" to 3" x 2" – DN 25 x DN 25 to DN 80 x DN 50)

DESCRIPTION

The ADCAMat POP pressure operated pump is recommended in the transfer of steam condensate, oils and other non-hazardous liquids compatible with the construction, to a higher elevation or pressure. Under certain conditions, it can drain a closed vessel under vacuum or pressure. The pump can be operated using steam, compressed air or other gases, and is manufactured in carbon steel or stainless steel.

OPERATION

Liquid flows by gravity into the pump through an inlet check valve, lifting the float. At this point, the motive fluid intake valve is closed while the vent valve is open. As the float reaches its highest position the motive fluid intake valve opens and the vent valve closes, allowing the motive fluid to enter the pump body. The pressure in the pump builds up just enough to overcome backpressure.

The pressurized liquid opens the outlet check valve and the discharge starts. The liquid discharged may be quantified through a special counter, enabling the pump to function as a reliable flow meter.

When the float reaches its lower position the motive fluid intake valve closes and the vent valve opens allowing the liquid to fill the pump once again, repeating the cycle.

MAIN FEATURES

Hardened stainless steel wear parts.
High-endurance inconel springs.
Low filling head to minimize installation space.
No electric requirements or NPSH issues.
Suitable for hazardous environments.
Low running costs.

OPTIONS: Level gauge.
Stroke counters.

USE: To lift steam condensate and other liquids compatible with the construction.

AVAILABLE MODELS: POPS – carbon steel.
POPSS – stainless steel.

SIZES: 1" x 1", 1 1/2" x 1 1/2", 2" x 2" and 3" x 2".
DN 25 x 25, DN 40 x 40, DN 50 x 50 and DN 80 x 50.

CONNECTIONS: Flanged EN 1092-1 PN 16.
Flanged ASME B16.5 Class 150.
Female threaded ISO 7 Rp (threaded flanges).
Others on request.

INSTALLATION: Horizontal installation. An example is shown in Fig. 1. See IMI – Installation and maintenance instructions.

MOTIVE MEDIUM: Saturated steam, compressed air, nitrogen and other gases.



CE MARKING – GROUP 2 (PED – European Directive)

| PN 16 | Category |
|-----------|---------------|
| All sizes | 2 (CE marked) |

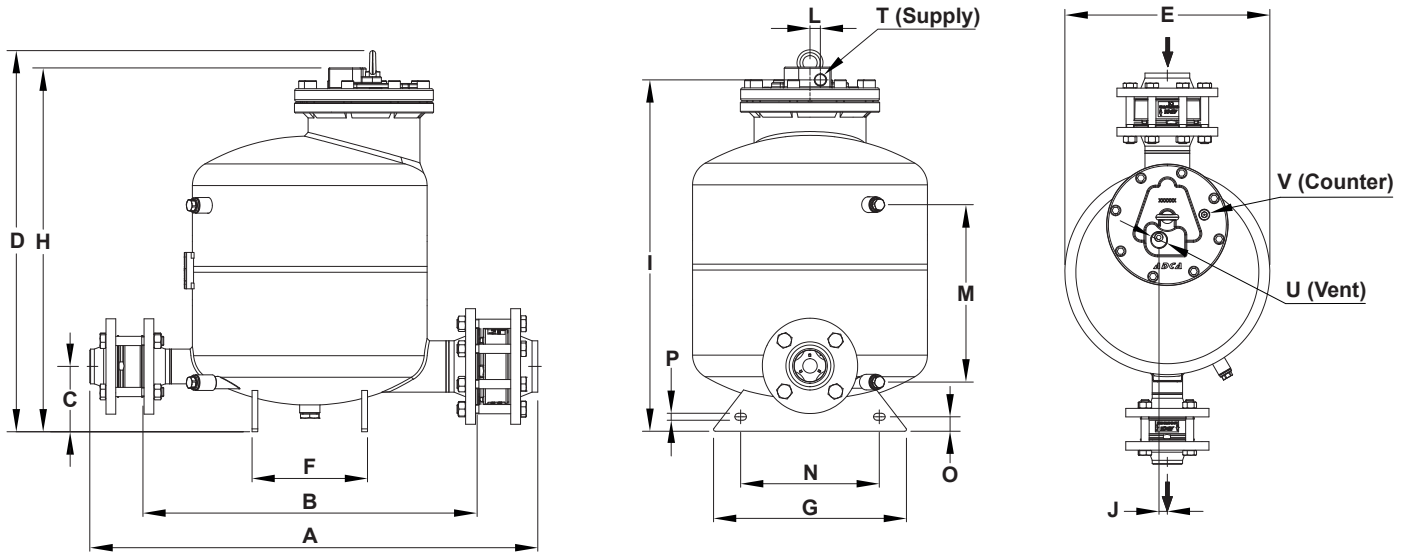
BODY LIMITING CONDITIONS *

| POPS | | | POPSS | | |
|-----------|---------------|--------------|-----------|---------------|--------------|
| | ALLOW. PRESS. | RELAT. TEMP. | | ALLOW. PRESS. | RELAT. TEMP. |
| PN 16 | 16 bar | 50 °C | PN 16 | 16 bar | 50 °C |
| | 14 bar | 100 °C | | 15 bar | 100 °C |
| | 13 bar | 195 °C | | 12,7 bar | 200 °C |
| | 12 bar | 250 °C | | 12 bar | 250 °C |
| CLASS 150 | 16 bar | 50 °C | CLASS 150 | 15,3 bar | 50 °C |
| | 14 bar | 100 °C | | 13,3 bar | 100 °C |
| | 13 bar | 195 °C | | 11,1 bar | 200 °C |
| | 12 bar | 250 °C | | 10,2 bar | 250 °C |

* Rating according to EN 1092-1:2018.

LIMITING CONDITIONS

| | |
|---|-----------|
| Liquid specific gravity | 0,8 to 1 |
| Maximum viscosity | 5° Engler |
| Maximum motive inlet pressure | 10 bar |
| Minimum motive inlet pressure | 0,5 bar |
| Maximum operating temperature | 185 °C |
| Minimum operating temperature | 0 °C |
| Pump discharge per cycle | 16 L |
| Pump discharge per cycle (3" x 2" – DN 80 x 50) | 25 L |



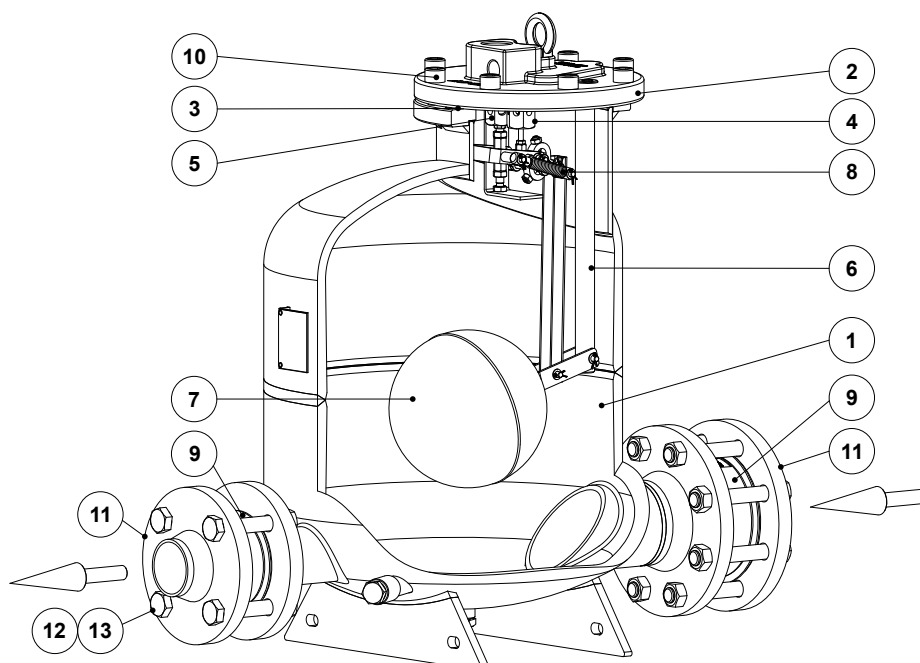
DIMENSIONS (mm)

| SIZE | A * | B * | C | D | E | F | G | H | I | J | L | M | N | O | P | T ** | U ** | V ** | WGT. (kg) | VOL. (L) |
|-------------------------------|-----|-----|-----|-----|-----|-----|-----|-----|-----|----|----|-----|-----|----|----|------|------|------|-----------|----------|
| 1" x 1" DN 25 x 25 | 578 | 444 | 100 | 640 | 323 | 160 | 244 | 617 | 598 | 17 | 18 | 327 | 150 | 25 | 12 | 1/2" | 1" | 1/2" | 68 | 31,7 |
| 1 1/2" x 1 1/2" DN 40 x 40 | 615 | 454 | 100 | 640 | 323 | 160 | 244 | 617 | 598 | 17 | 18 | 327 | 150 | 25 | 12 | 1/2" | 1" | 1/2" | 72,7 | 31,8 |
| 2" x 2" DN 50 x 50 | 644 | 460 | 100 | 640 | 323 | 160 | 244 | 617 | 598 | 17 | 18 | 327 | 150 | 25 | 12 | 1/2" | 1" | 1/2" | 76,5 | 31,9 |
| 3" x 2" DN 80 x 50 | 776 | 580 | 113 | 650 | 406 | 200 | 334 | 627 | 608 | 17 | 18 | 327 | 240 | 25 | 12 | 1/2" | 1" | 1/2" | 95,8 | 48,9 |

* With EN 1092-1 welding neck flanges. Dimensions may differ if ASME B16.5 flanges or ISO 7 Rp female threaded flanges are requested. Consult the manufacturer.

** As standard, in versions manufactured with EN 1092-1 PN 16 flanges, these connections are female threaded ISO 7 Rp. In versions with ASME B16.5 flanges, these connections are female threaded NPT.

MATERIALS



| MATERIALS | | | |
|-----------|-------------------------------|---|---|
| POS. N° | DESIGNATION | POPS | POPSS |
| 1 | Pump body | P265GH / 1.0425; P235GH / 1.0345; S235JR / 1.0038; P250GH / 1.0460 | AISI 316 / 1.4401; AISI 304 / 1.4301 |
| 2 | Cover | WCB / 1.0619 | A351 CF8M / 1.4408 |
| 3 | * Cover gasket | Stainless steel / Graphite | Stainless steel / Graphite |
| 4 | * Intake valve/seat assembly | Stainless steel | Stainless steel |
| 5 | * Exhaust valve/seat assembly | Stainless steel | Stainless steel |
| 6 | Lever assembly | Stainless steel | Stainless steel |
| 7 | * Float | Stainless steel | Stainless steel |
| 8 | * Spring assembly | Inconel | Inconel |
| 9 | * Check valve | A351 CF8M / 1.4408 | A351 CF8M / 1.4408 |
| 10 | Bolts | Steel 8.8 | Stainless steel A2-70 |
| 11 | Counter flanges | P250GH / 1.0460 | AISI 316 / 1.4401 |
| 12 | Bolts | Zinc plated steel | Stainless steel A2-70 |
| 13 | Nuts | Zinc plated steel | Stainless steel A2-70 |

* Available spare parts.

SIZING

To accurately size a pressure operated pump, the following information must be provided:

1. The condensate load (kg/h).
2. The operating medium (steam, compressed air or other gases) and its pressure.
3. The total lift or backpressure in bar the pump will have to overcome. This includes the change in fluid level elevation after the pump (0,0981 bar/m of lift), plus pressure in the return piping, plus the pressure drop caused by pipe friction and other system components.
4. Available filling head in mm or any other dimension that allows its determination.

Table 1

| CAPACITY CORRECTION FACTOR FOR GASES OTHER THAN STEAM | | | | | |
|---|------|------|------|------|------|
| % Backpressure vs Motive pressure (BP/MP) | 10% | 30% | 50% | 70% | 90% |
| Correction factor | 1,04 | 1,08 | 1,12 | 1,18 | 1,28 |

Table 2

| CAPACITY CORRECTION FACTORS FOR FILLING HEADS OTHER THAN 300 mm | | | | |
|---|-------------------|-----|------|------|
| PUMP SIZE | FILLING HEAD (mm) | | | |
| | 150 | 300 | 600 | 900 |
| 1" x 1" – DN 25 x 25 | 0,7 | 1 | 1,2 | 1,35 |
| 1 1/2" x 1 1/2" – DN 40 x 40 | 0,7 | 1 | 1,2 | 1,35 |
| 2" x 2" DN 50 x 50 | 0,7 | 1 | 1,2 | 1,35 |
| 3" x 2" – DN 80 x 50 | 0,9 | 1 | 1,08 | 1,2 |

RECEIVER

A receiver is recommended to temporarily hold the liquid and prevent any flooding of the equipment, while the pump is performing a pumping cycle. A definable length of large diameter pipe can be used. Suggested receiver sizes are shown in Table 3.

Table 3

| RECEIVER | | | | |
|---------------------------|----------------------|------------------------------|----------------------|----------------------|
| PUMP SIZE | 1" x 1" – DN 25 x 25 | 1 1/2" x 1 1/2" – DN 40 x 40 | 2" x 2" – DN 50 x 50 | 3" x 2" – DN 80 x 50 |
| Pipe size with 1 m lenght | 6" | 6" | 8" | 10" |

Table 4

| FLOW RATE (kg/h) INSTALLATION WITH 300 mm FILLING HEAD ABOVE THE PUMP COVER | | | | | |
|--|------------------|----------------------|------------------------------|----------------------|----------------------|
| MOTIVE PRESS. (bar) | TOTAL LIFT (bar) | 1" x 1" – DN 25 x 25 | 1 1/2" x 1 1/2" – DN 40 x 40 | 2" x 2" – DN 50 x 50 | 3" x 2" – DN 80 x 50 |
| 1 | 0,35 | 840 | 1490 | 2320 | 4480 |
| 2 | | 1030 | 1520 | 3160 | 5240 |
| 3 | | 1140 | 1640 | 3560 | 5640 |
| 4 | | 1180 | 1680 | 3840 | 5840 |
| 5 | | 1240 | 1740 | 3910 | 5900 |
| 6 | | 1270 | 1760 | 3940 | 5980 |
| 8 | | 1300 | 2200 | 3990 | 6030 |
| 10 | | 1310 | 2205 | 4000 | 6080 |
| 2 | 1 | 805 | 1560 | 2550 | 4080 |
| 3 | | 940 | 1790 | 2990 | 4720 |
| 4 | | 1080 | 1930 | 3160 | 5080 |
| 5 | | 1110 | 2010 | 3200 | 5280 |
| 6 | | 1140 | 2090 | 3250 | 5400 |
| 8 | | 1180 | 2190 | 3280 | 5490 |
| 10 | | 1190 | 2200 | 3320 | 5560 |
| 3 | 2 | 780 | 1495 | 2470 | 3510 |
| 4 | | 900 | 1690 | 2620 | 3950 |
| 5 | | 1000 | 1820 | 2830 | 4230 |
| 6 | | 1040 | 1910 | 2860 | 4740 |
| 8 | | 1100 | 2010 | 2880 | 4880 |
| 10 | | 1110 | 2060 | 2900 | 4960 |
| 4 | 3 | 740 | 1400 | 2360 | 3480 |
| 5 | | 860 | 1545 | 2540 | 3640 |
| 6 | | 910 | 1675 | 2560 | 3720 |
| 8 | | 970 | 1805 | 2590 | 4050 |
| 10 | | 980 | 1850 | 2650 | 4110 |
| 5 | 4 | 720 | 1335 | 2280 | 2690 |
| 6 | | 820 | 1480 | 2460 | 2860 |
| 8 | | 910 | 1675 | 2500 | 3190 |
| 10 | | 930 | 1760 | 2540 | 3380 |
| 6 | 5 | 680 | 1290 | 2080 | 2520 |
| 8 | | 740 | 1530 | 2180 | 2740 |
| 10 | | 810 | 1630 | 2220 | 2860 |
| 7 | 6 | 660 | 1230 | 1880 | 1940 |
| 8 | | 730 | 1370 | 1940 | 2240 |
| 10 | | 820 | 1490 | 2150 | 2360 |

Remark: Based on liquid specific gravity of 0,9 to 1,0.

Example

Condensate load 1800 kg/h
 Filling head 150 mm
 Motive fluid Compressed air
 Available pressure 8 bar
 Vertical lift after pump 6 m
 Return piping pressure 1,5 bar
 Piping friction pressure drop Negligible

Filling head correction:
 With 150 mm filling head the correction factor from Table 2 is 0,7. The corrected capacity is thus 2590 kg/h x 0,7 = 1813 kg/h.

Calculations:

Total backpressure: 1,5 bar + (6 m x 0,0981) = 2,09 bar.
 Assuming steam as motive medium at a pressure of 8 bar and a total backpressure of 3 bar, then according to Table 4 a DN 50 x 50 pump, with a capacity of 2590 kg/h, is the recommended size.

Correction for air as a motive medium:

The % backpressure is 2,09 bar / 8 bar = 30%.
 The correction factor from Table 1 is 1,08.
 The corrected capacity is thus 1813 kg/h x 1,08 = 1958 kg/h, and so, a DN 50 x 50 pump is still the recommended size.

TYPICAL APPLICATIONS

CONDENSATE RECOVERY IN A OPEN LOOP SYSTEM

The pump transfers high temperature condensate without cavitation problems.

The vent line must be unrestricted and self draining to the receiver (Fig. 1).

| MATERIALS | | | |
|-----------|----------------|---------|----------------|
| POS. N° | DESIGNATION | POS. N° | DESIGNATION |
| 1 | Heat exchanger | 6 | Check valve |
| 2 | Receiver | 7 | Steam trap |
| 3 | Shut-off valve | 8 | Air vent |
| 4 | Y strainer | 9 | Overflow |
| 5 | Pump | 10 | Vacuum breaker |

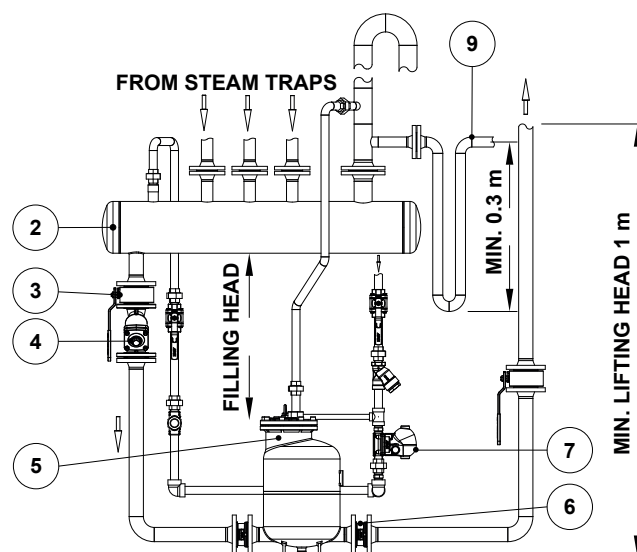


Fig. 1

REMOVAL OF CONDENSATE UNDER PRESSURE WITH PUMP AND STEAM TRAP COMBINATION

The pump is installed in a closed loop with its vent connected to a pressurized receiver (Fig. 2).

When steam pressure is sufficient to overcome backpressure, the steam trap operates. As soon as, e.g., the equipment's control valve starts to modulate, the steam pressure will decrease (even vacuum can occur). The lower differential pressure decreases the steam trap ability to discharge, causing the condensate level to rise inside the body of the pump. Once the pump float reaches its higher position, the intake valve opens and steam replaces the necessary positive pressure to pump out the condensate.

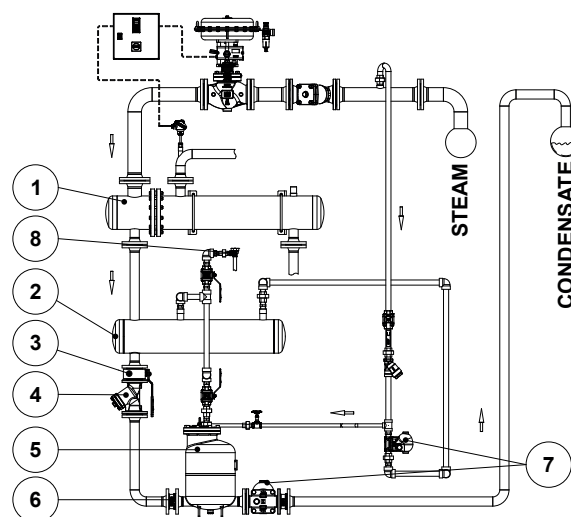


Fig. 2

DRAINAGE OF A SINGLE UNIT UNDER VACUUM

This configuration works with units operating with a minimum absolute pressure of 0,2 bar (Fig. 3).

For proper operation the filling head (H1) must range between 1 and 2 meters. The lift (H) must be as minimum as possible, but never less than 1 meter, otherwise a siphon with height (H2) is required.

Steam must be used as motive medium, and its maximum pressure should not exceed 3 bar.

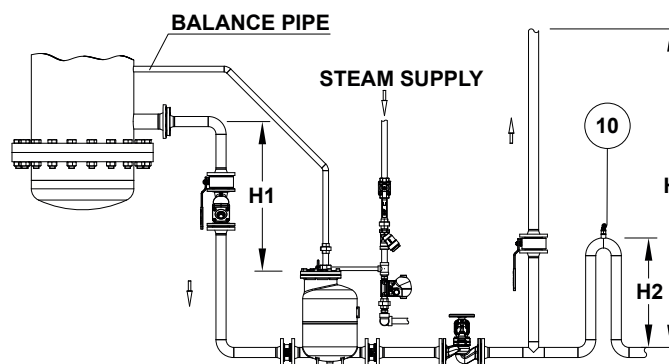


Fig. 3